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AABC Commissioning Group

AIA Provider Number 50111116



## Fundamentals of Test & Balance for Engineers, Cx & Energy Providers

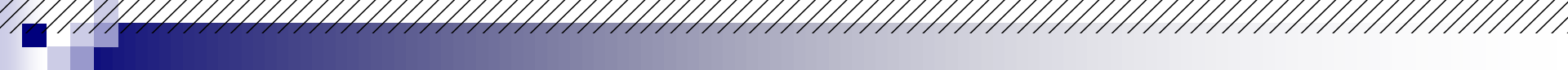
Course Number: CXENERGY1719

***Jim Hall, P.E., TBE, CxA***  
***Systems Management & Balancing, Inc.***

April 26, 2017

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Questions related to specific materials, methods, and services will be addressed at the conclusion of this presentation.

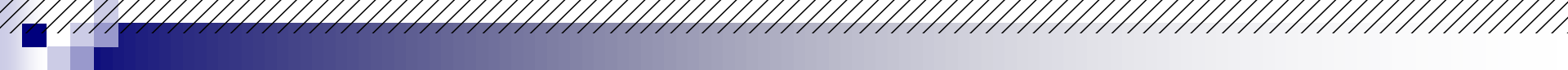
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# Course Description

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This practical information-packed session will explain many of the key test and balance issues—from precise specifications, to duct leakage testing, to pump- and fan-curve considerations—that if properly addressed in cooperation with an independent TAB firm can ensure that any project goes smoothly.



# Learning Objectives

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At the end of the this course, participants will be able to:

1. Understand the proper use, application, and limitations of the TAB instrumentation.
2. Understand what is accurate, useful and meaningful data that is obtained in the field vs. laboratory data for use on their project.
3. Gain an understanding of HVAC systems and the TAB/measurement process; how can systems be set up to allow for proper data collection.
4. Promote a project team approach to address schedule challenges, design alternatives as it relates to balancing device locations, equipment usage and HVAC system operation.

The majority of the presentation covers **air systems**, if time permits there are a few slides at the end on **water systems** that can be reviewed.

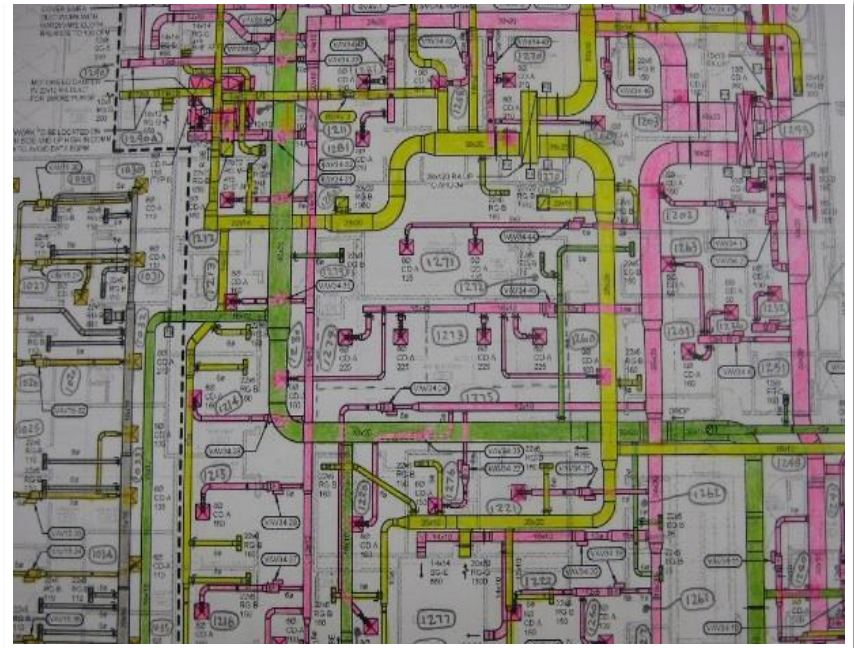
# Learning Laboratories

- The TAB Agency is fortunate....every project is a potential Learning Laboratory
- We are not promoting “shortcuts”, we are trying to share experiences for improving industry knowledge
- Lessons learned need to be shared



# Project Document Review

- **TAB Data** is a byproduct of:
  - System Design
  - Equipment Selection
  - System Installation
  - System Operation
  - Proper use of the TAB instrumentation



# Project Document Review

## Project Planning

- One of the most beneficial and productive parts of the TAB & Cx process is a **specification and drawing review**
- **START EARLY** – During or before design if possible
- Utilize **common sense**; what is the goal or intent?
- Review **system functionality**; Are balancing dampers & valves strategically placed? Is there proper access to equipment/systems?
- If the CxA is utilizing the project specifications to establish PFC's and FPT's make sure they are applicable – A **Project Specific Specification**



# Project Document Review

## TAB Data

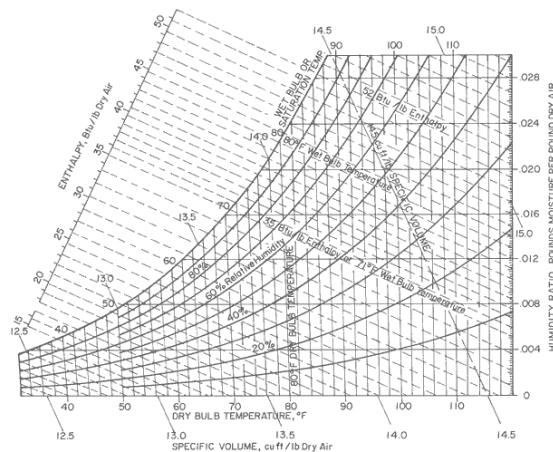
- Understand what is **meaningful data**. Discuss with the design professional if the specified data is relevant or useful.
- Will the data **benefit the owner and project?**
- Try to think of **how data will be obtained and what data will be required.**
- Do not get hung up on getting data/numbers, **think system!!**



# Project Document Review

## TAB Data

- Will the requested data be Accurate, Repeatable and Meaningful?
  - Example – Wet-bulb temperatures
    - Can a latent load be established?
    - Temperature traverse is required, not a single point temperature measurement.
    - Maintain the proper air velocities
    - Maintain proper water flow and water temperatures



# Project Document Review

## System Design/Equipment Selection

- Can outdoor air be measured to AHU?
  - Is there enough ductwork for a proper traverse?
  - Does unit configuration allow for proper measurement?
- Can outdoor air be measured to RTU?
  - Is the RTU configured/installed for outdoor air measurement?
  - If mixed air temperature method is utilized can an accurate mixed air temperature be measured?
  - Static pressure profile of RTU or outdoor duct/equipment; make sure “factory or weatherproof test ports” are installed.



# Project Document Review

## System Design/Equipment Selection/TAB Instrumentation Airflow Measurement – Traverse Locations

- The **primary/preferred** airflow measurement method is a **duct traverse**.
- **Ideal traverse plane:**
  - For **round duct**, AABC, AMCA & ASHRAE all identify the ideal traverse plane as **2 ½ diameters from condition** (discharge, elbow, etc.) for up to 2500 fpm. Add 1 diameter for each additional 100 fpm.
  - For **rectangular duct**,  $E_L = (4a*b/\pi)^{0.5}$ , where “a” & “b” are the duct dimensions.
  - Accuracy of the traverse is better at 1000 fpm or above.

# Project Document Review

## System Design/Equipment Selection/TAB Instrumentation Airflow Measurement – Traverse Locations

### Example:

- 10,000 cfm, 30" x 20" duct, 2400 fpm
- $E_L = (4a*b/\pi)^{0.5} = 27.6"$   
 $2\frac{1}{2} * 27.6" = 69.1"$
- 69.1" (~ 6') straight duct required



# Project Document Review

## System Design/Equipment Selection

### Traverse Locations Alternatives

A duct traverse can still be performed if an ideal traverse plane is not available.

- A traverse plane is suitable for flow measurements if more than 75 % of the velocity pressure readings are greater than 1/10 of the maximum velocity measurement and are not negative
- Use **TAB instrumentation correctly**; a thermal anemometer does not measure unidirectional

### **Alternatives to Traverse**

**Only if a duct traverse is NOT accurate:**

- Face velocity reading of filters, coils, etc.
- Summation of airflows at individual outlets
- Summation of calibrated VAV boxes as read at the DDC computer

# Project Document Review

## Traverse Locations - System Effect

### ASHRAE Journal Feb 2006 Article

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## System Effect



By Bernard Ratledge, Life Member ASHRAE

For a building owner concerned with operating costs, the clearest way to document that the M&E consultant, mechanical contractor and testing, adjusting, balancing (TAB) contractor have achieved the design energy consumption is to compare the energy consumption given in the TAB equipment report with that specified in approved shop drawings.

From energy bills received for 50 new schools in Ontario, Canada (part of the 137 schools in the Dufferin-Peel Catholic district), it was evident that considerable difference existed between the predicted en-

ergy consumption and actual consumption for installed equipment. Most notable was the difference in power being consumed by fan systems, prompting further investigation of the data in the TAB report.

Unsurprisingly, the investigation revealed that at the speed measured the reported fan volume and static pressure points did not intersect on the fan performance curve at the measured speed. A considerable difference existed between the measured and true static pressure indicated on the fan performance curve that could only be attributed to the presence of a system effect factor (SEF) after all recorded data was checked for accuracy.

**About the Author**  
Bernard Ratledge is a building systems engineer with Dufferin-Peel Catholic District School Board in Mississauga, ON, Canada. He is a member of ASHRAE Guideline Project Committee (GPC) 1, the HVAC Commissioning Process, and ASHRAE GPC 4, Preparation of Operating and Maintenance Documentation for Building Systems.

### How to Avoid This Increased Operating Cost?

- By not trying to save dollars per square foot by reducing the size of the mechanical room. The increased operating cost of the poor installation is likely to be far greater than the cost of providing the space necessary to ensure a good ductwork installation.

The increase in fan bhp =  $16.83 - 10.06 = 6.77$  (12.55 kW - 7.5 kW = (5.05 kW).

Using the same operating parameters as Example 1:

Based on the fan operating 245 days  $\times$  8 hrs/day  $\times$  7.5 = 14,700 kWh  $\times$  \$0.06/ kWh = \$882 + 7.5  $\times$  \$10/kW demand  $\times$  12 = \$1,782/yr base electric cost. Revised operating cost with new motor = 245 days  $\times$  8 hrs/day  $\times$  12.55 = 24,598 kWh  $\times$  \$0.06/ kWh = \$1,475.88 + 12.55  $\times$  \$10/kW demand  $\times$  12 = \$2,981.88/yr or \$1,199.88/yr increase. A life-cycle analysis based on a school useful life of 25 years, annual energy cost escalation 5%, shows an estimated total additional operating cost of \$86,489.





# Project Document Review

## System Design/Equipment Selection

### Airflow Measurement & Fan Curves

#### ■ Fan curves

- ☐ AMCA Tested
- ☐ Produced under **laboratory conditions**
- ☐ Free inlet
- ☐ Straight discharge
- ☐ Ideal traverse plane
- ☐ Multiple speeds-extrapolated data
- ☐ Standard temperature & pressure (STP)
- ☐ Normal manufacturing tolerances

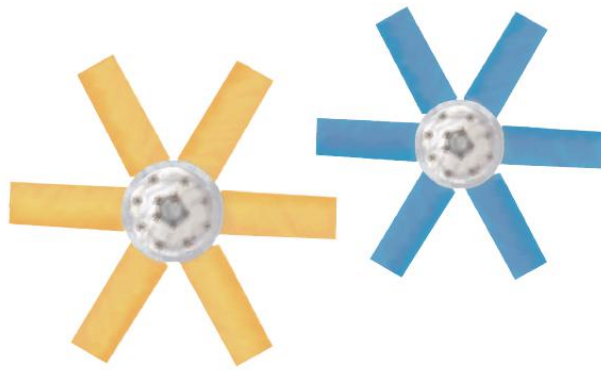
#### ■ Know the **limitations** of fan curves



# Airflow Measurement & Fan Curves

## ASHRAE Journal Article, November 2005

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### Fan Data

Is What You See,  
What You Get?

By Kim G. Osborn, Associate Member ASHRAE

It happens occasionally that even after taking great care in design, the air handler turns out to be louder than expected or the airflow is less than design. This article examines some discrepancies that can occur between catalog data and the actual performance.

At first it might seem strange that, with well-established testing standards, major differences can exist between the catalog data and the performance of the fan in application. A number of reasons exist for this.

Not every wheel size is tested, and those tested are run at a limited number of speeds. Fan testing is time consuming and

expensive. It is generally not practical to test all sizes or to test each size at a large number of speeds. Fan engineers strive to present the most reliable selection information they can, but due to gaps in the test series, not all sizes and operating points may be reliable. The end result is that you might take great pains to design an HVAC system with critical sound

and/or airflow issues, and substantially miss the design criteria because the fan data used was too optimistic.

It is becoming more important to be able to predict and control HVAC sound. Key to this goal is knowing the sound power spectrum of the fans used in the equipment. The designers then must either depend on the catalog data for the fans selected or measure the fans' sound power themselves. For designers without an available acoustical laboratory, the latter option is often too costly. Therefore, the only option is to use the catalog numbers.

—About the Author  
Kim G. Osborn is C3S laboratory manager at Governor Corporation, Oklahoma City.

it is rare to find 25 ft (7.6 m) of straight duct on a fan in real-world applications. Most of the differences are probably the result of unidentified system effects and what is sometimes called manufacturing variances.

The most dramatic difference between the test data and catalog data is shown in Figure 2. This shows the measured airflow

data for two nearly identical 36.5 in. (927 mm) DWDI fans and compares these to the catalog data. The two test fans used the same size and design of wheels, inlet cones, and scrolls but had minor differences in the support frame design. Not only did these two “identical” fans have noticeably different airflow, but both fell substantially short of the cataloged airflow curve.

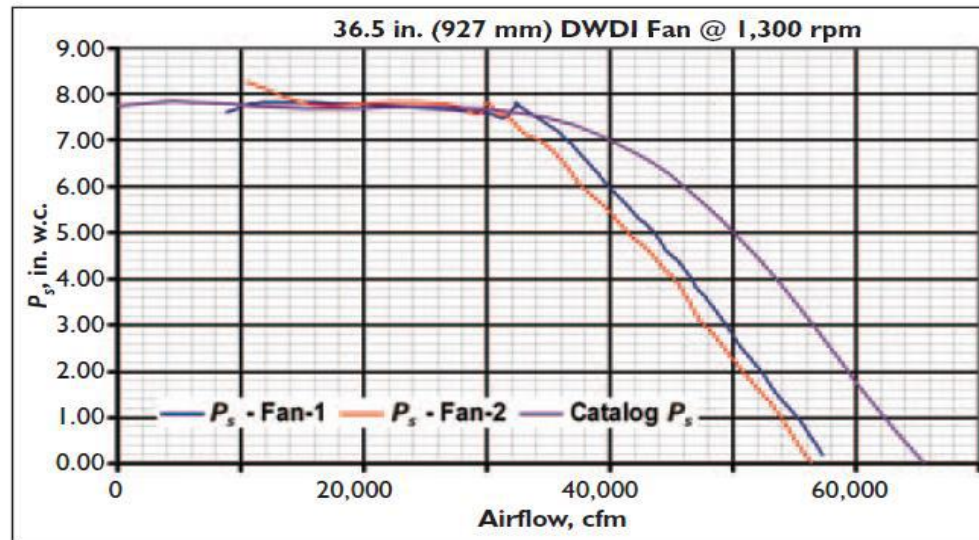


Figure 2: Measured fan airflow data compared to catalog data.

# Project Document Review

## System Design/Equipment Selection

### Airflow Monitoring Stations

- ❑ Requires calibration and maintenance
- ❑ Requires filtered air
- ❑ Will the AFMS work properly in the installed location? Is the velocity profile acceptable?
- ❑ Will the AFMS work at minimum airflow and maximum airflow or vice-versa?
- ❑ Will the control damper create turbulence and measurement issues?



# Project Document Review

## System Design/Equipment Selection

### Measurement Tolerances

#### ■ Think about $\pm 5\%$ or 0% to +10% tolerances

- May not be feasible, depending on the system and its components.
  - 0% to +10%; Is this realistic for how the system operates? What are the DDC System's control tolerances?
- Keep in mind, that in Labs and ORs, the main criteria for airflow is ACH and room pressurization. Typically the room envelope dictates the amount of airflow required to maintain proper room pressurization.
- The TAB equipment manufacturer's tolerances sometimes are greater than the specification tolerances.



# Project Document Review

## System Design/Equipment Selection

### Measurement Tolerances

AABC National Standards 7<sup>th</sup> Edition Section 2.8

- Fans -5% to +10%

**Figure 2.2 Percent Tolerance Between Air Terminals Within a Space**

Classification	Number of Terminals in the Space		
	1	2	3 or More
General	±10%	±10%	±15%
Warehouse or Industrial	±10%	±15%	±15%
Operating room or other special environmental rooms	±5%	±5%	±10%

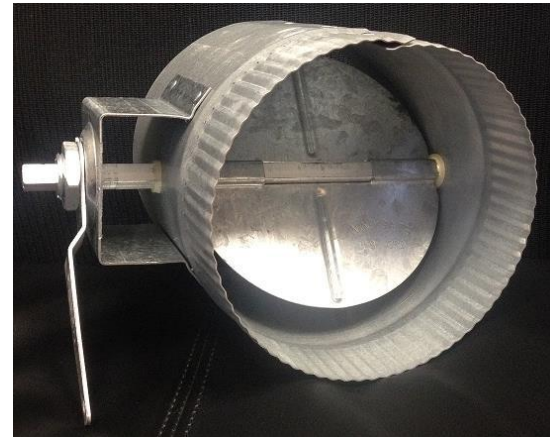
If the plan design is less than 100 CFM, the diffuser shall be adjusted to within 10 CFM.

# Project Document Review

## System Design/Equipment Selection

### Balancing Dampers

- What is specified? What is installed? This can affect the TAB tolerances and system performance.





# Project Document Review

## System Design/Equipment Selection

### Balancing Dampers & Grills

- Accurate airflow measurement can be challenging on surface mounted grills
- **Never** rely on **face dampers** for air balancing
  - Face dampers add static to a system, but do not help divert airflow within the system
  - Can go closed or open due to system pressure
  - Can be noisy, the occupant can adjust, & they get dirty on exhaust systems
  - Required airflow tolerances are difficult to obtain



# Project Document Review

## System Design/Equipment Selection

### Insulation Requirements

- Make sure damper handles are exposed on externally wrapped ductwork



- Utilize test port extensions on balancing valves and all test ports

# Project Document Review

## System Design/Equipment Selection

### Control Systems

- Make sure that access to the control system is made available to the TAB agency and CxA. This includes any required hardware and software.
- Know when the system “Front End” will be operational (sometimes the owner provides this hardware and/or network/internet connection)
- This seems to be a regional issue, not a manufacturer’s issue.





# Project Document Review

## System Design/Equipment Selection

### Domestic & Lab Water Systems

- **Plumbing Pumps, Fire Pumps, Steam Condensate Pumps**

Typically these type of systems cannot be accurately tested without a constant, established water flow.



# Project Document Review

## System Design/Equipment Selection

### Domestic & Lab Water Systems

- A non-invasive procedure is recommended
  - Ultrasonic Flow Meter
  - Pipe surface temperature
  - Permanently installed gauges and/or thermometers
- A balancing valve is still required to allow for proportioning of the water system
- Consider installing temperature sensors on the domestic hot water recirculation loop that can report the temperatures to the DDC system

#### Shortridge Owner's Manual

##### 1.0 SAFETY WARNINGS

READ ALL SAFETY WARNINGS CAREFULLY BEFORE USING HYDRODATA MULTIMETER.

Do not use the HydroData Multimeter or accessories on potable (drinkable) water or on any other fluid systems which may be used for human or animal consumption (or which may otherwise cause a health risk) because of the possibility of the system being tested becoming contaminated by residue from within the meter, piping or hoses.

The HydroData Multimeter and Valve Network Panel are designed for pressure measurement of non-potable water and air hydraulic and hydronic systems. This meter is not designed for and must not be used with potentially hazardous fluids or connected to any pressure source greater than 250 psi.

Do not use the HydroData Multimeter or Valve Network Panel to measure steam or high temperature hot water systems, or with acid, caustic, or any other hazardous chemicals.

#### Safety

#### Alnor Owner's Manual



- The HM 650 is intended for use on hydronic heating and cooling systems only. Never use the instrument on potable water systems or other systems which may be used to convey fluids or air for human or animal consumption.
- Never use the HM 650 to measure the pressure of volatile, flammable, or otherwise hazardous fluids or gases. The instrument is not designed to be intrinsically safe nor is it intended for use with caustic or corrosive chemicals.
- Never use the HM 650 on steam or temperatures greater than (100°C; 212°F) water.
- Always observe proper safety precautions and wear the appropriate personal protective equipment when working on high pressure systems. Ruptured
- Use caution as you release the water or air pressure when disconnecting the instrument to lessen the risk of water spray and personal injury.
- Exercise appropriate caution when using the HM 650 near electrical devices. Water spray when bleeding or disconnecting the high and low pressure lines poses a potential risk of severe personal injury and/or damage to equipment.
- Never connect the HM 650 to systems which exceed the instrument's maximum pressure specification (300 PSI; 2068 kPa).
- Always thoroughly drain and dry the HM 650's hoses and internal piping after use. This will help prevent accidental spills as well as the growth of hazardous microorganisms.

# Project Document Review

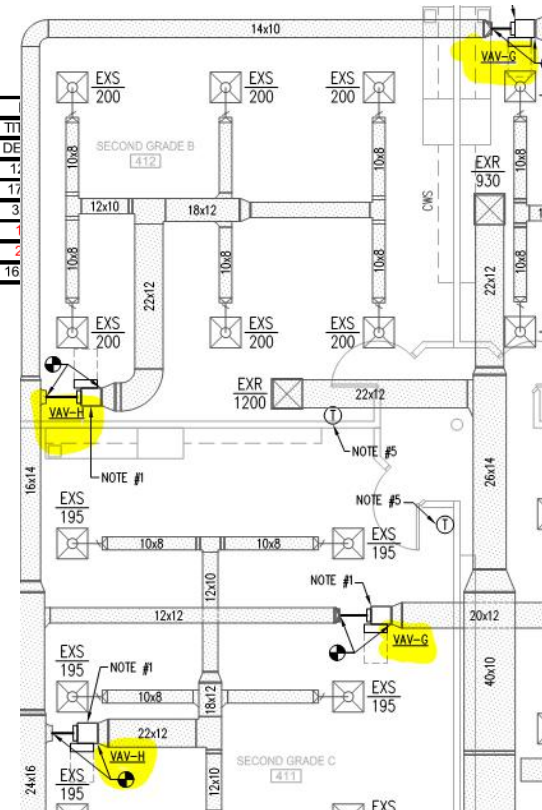
## System Design/Equipment Selection

### Drawing Nomenclature & Equipment ID

- Help promote identifying each piece of equipment (fans, AHUs, HPs, VAVs, Pumps, etc.) with a **unique tag**.

**VARIABLE AIR VOLUME TERMINAL UNIT SCHEDULE**

UNIT TAG	A	B	C	D	E	F	G	H
MANUFACTURER	TITUS	TITUS	TITUS	TITUS	TITUS	TITUS	TITUS	TITUS
MODEL NUMBER	DESV	DESV	DESV	DESV	DESV	DESV	DESV	DESV
INLET SIZE	40	50	60	70	80	90	100	120
BOX MAXIMUM AIRFLOW (C.F.M.)	150	200	300	450	600	850	1150	1700
BOX MINIMUM AIRFLOW (C.F.M.)	45	65	85	115	150	195	245	360
MAXIMUM NOISE LEVEL - DISCHARGE (NC)	11	11	10	13	17	15	18	21
MAXIMUM NOISE LEVEL - RADIATED (NC)	<15	<15	13	15	17	14	20	22
BOX DISCHARGE DUCT CONNECTION SIZE	12x8	12x8	12x8	12x10	12x10	14x12	14x12	16x12

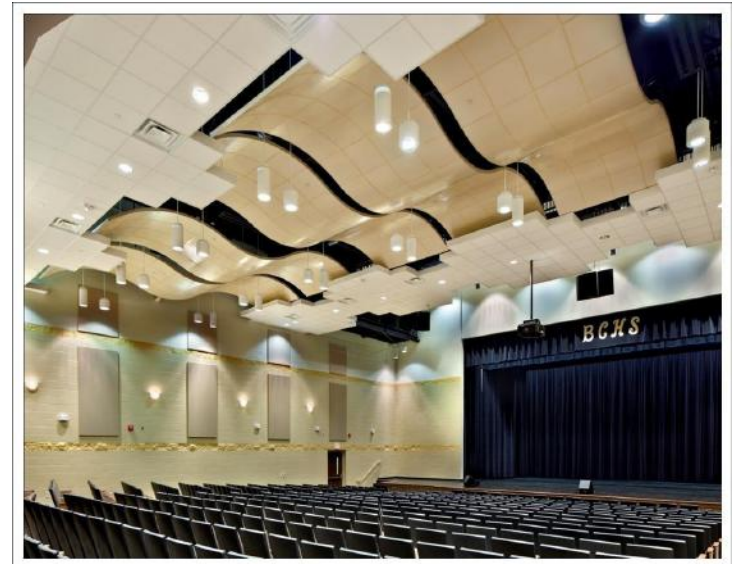


# Project Document Review

## System Design/Equipment Selection

### Access Challenges

- Proper clearance and access must be provided to all dampers, valves, equipment, etc.
  - Sheetrock ceilings, architectural features, etc.
  - Locate devices in the corridors outside of OR's, classrooms, etc.
- Access to outlets, dampers, etc. in theatre type seating areas. How will this be accomplished? AHU is typically not in operation when scaffolding is installed.





# TAB Instrumentation

## The Flow Hood

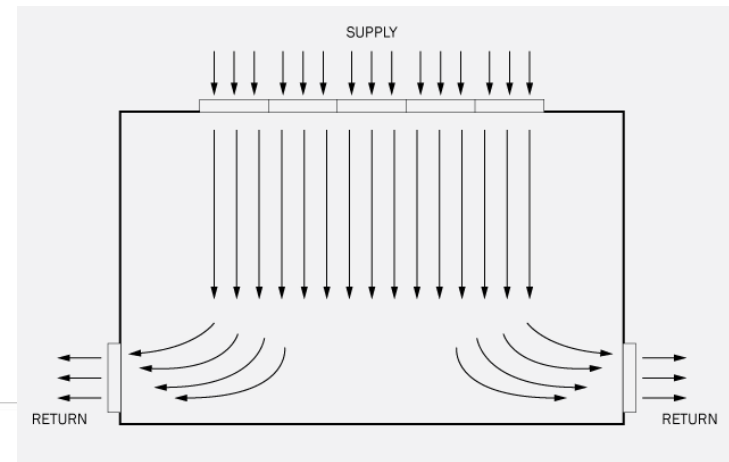
- The flow hood is a **proportioning device**.
- Know the **limitations** of the flow hood and how it should be used



# TAB Instrumentation

## The Flow Hood

- Note: The Flow Hood may **require the development and use of correction factors** when used on swirl diffusers, or on other types of diffusers with uneven air throw. The Flow Hood may not be appropriate for use on small supply outlets at high jet velocities or “nozzle” type outlets. These outlets cause an extreme concentration of air velocity on portions of the flow sensing grid. The **Flow Hood readings may be inaccurate under such conditions.** (Shortridge Instruments owners manual)

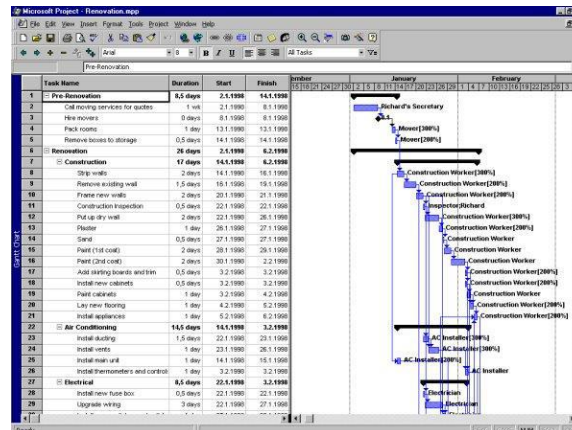


# Scheduling Challenges

- There needs to be enough time allowed in the schedule for the TAB & Cx work to be completed. Request TAB durations early in the scheduling process.
- All work must be complete for TAB work to commence.
  - ☐ Clean air filters installed.
  - ☐ All strainers cleaned and start-up strainers removed.
  - ☐ All balancing dampers installed and 100% open.
  - ☐ All manual balancing valves and flow measuring stations installed and 100% open.
  - ☐ Temperature Controls complete and functional.

# Scheduling Challenges

- Remember that TAB work is completed **by system, not by area**.
  - HVAC systems are typically “Vertical” and buildings are finished “horizontal”
  - Very seldom does the HVAC system match the “Phasing or Scheduled Areas.”
- Make sure that the Owner & Architect understand the possibility that the TAB work might be performed after occupancy.
- Variable volume systems (air and water) can have provisions to balance partial HVAC systems. Constant volume systems can pose major complications if they overlap several areas/phases.
- Hydronic systems need to be carefully considered for scheduling issues.





# TAB Reports

- Typically a final TAB report is NOT available at time of commencement of the Cx FPT's.
- Have an experienced, responsible engineer review the report. It is not just about **matching numbers**. It is reviewing system performance and employing engineering judgment.
- Don't hesitate to call the TAB agency to review the report together or ask questions.
- **Keep in mind that there is no benefit to the TAB Agency to report problems or deficiencies, it is a responsibility. Be cautious of the “pristine” TAB report.**

# This concludes The American Institute of Architects Continuing Education Systems Course

## Fundamentals of Test & Balance for Engineers, Cx & Energy Providers

Course Number: CXENERGY1719

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# Additional Information

If there is time available the following slides will be reviewed.

# Water Flow Measurement: Pump Curves

## Design Requirements:

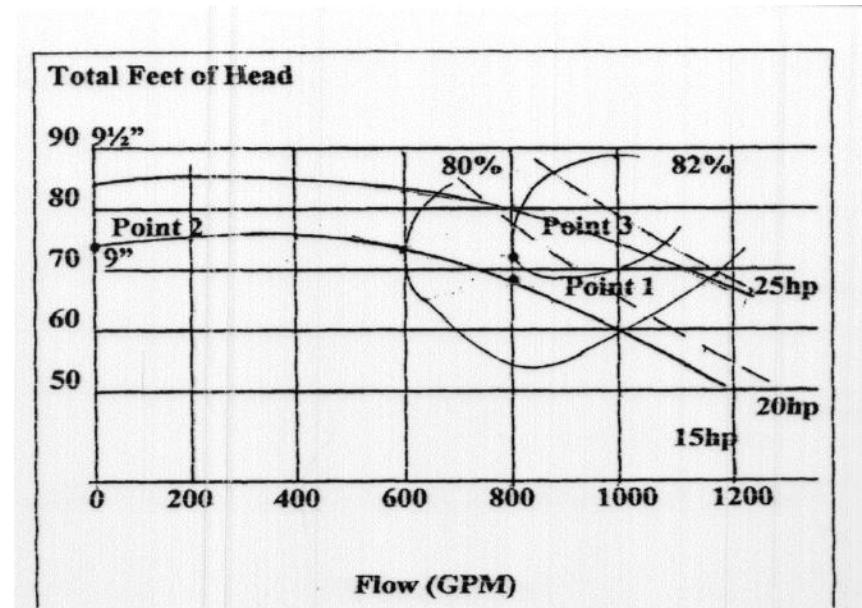
- 800 gpm @ 68'  
9" Impeller, 20 hp motor,  
5BC, 1750 rpm (Point 1)

## Field Measurements:

- Shutoff  $\Delta P = 73'$  (Point 2)
- Operating  $\Delta P = 70.0'$

## Results:

- Actual: 700 gpm w/9" imp
- 12.5% below design
- Flat Pump Curve – Hard to interpolate.
- Utilize measured flows at terminals or branches to determine pump total.



# Water Flow Measurement: Pump Curves

## Design Requirements:

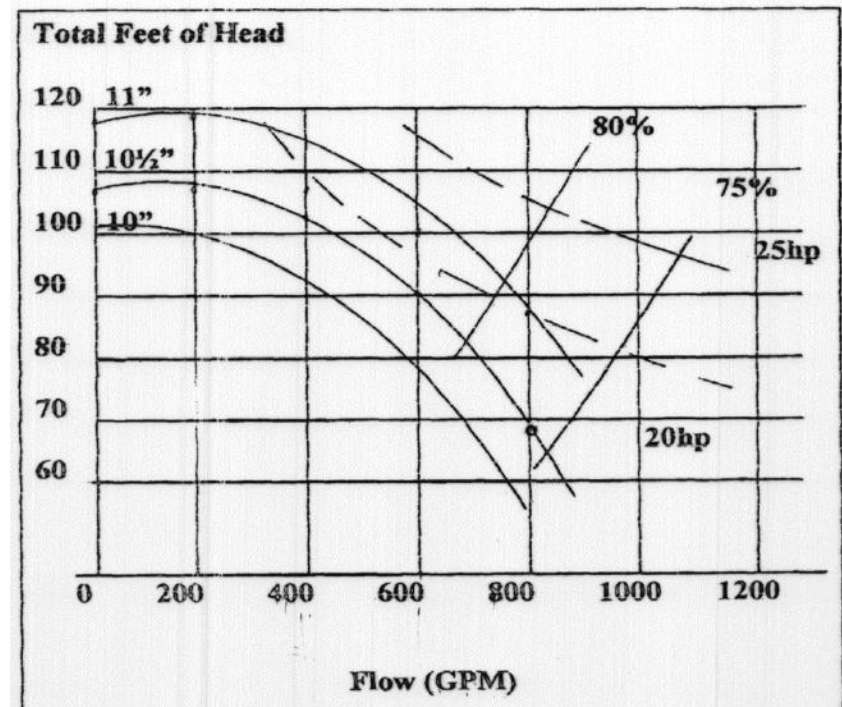
- 800 gpm@ 68'  
10-3/8" Impeller, 20 hp motor,  
4E, 1750 rpm

## Field Measurements:

- Shutoff  $\Delta P = 104'$
- Operating  $\Delta P = 72'$

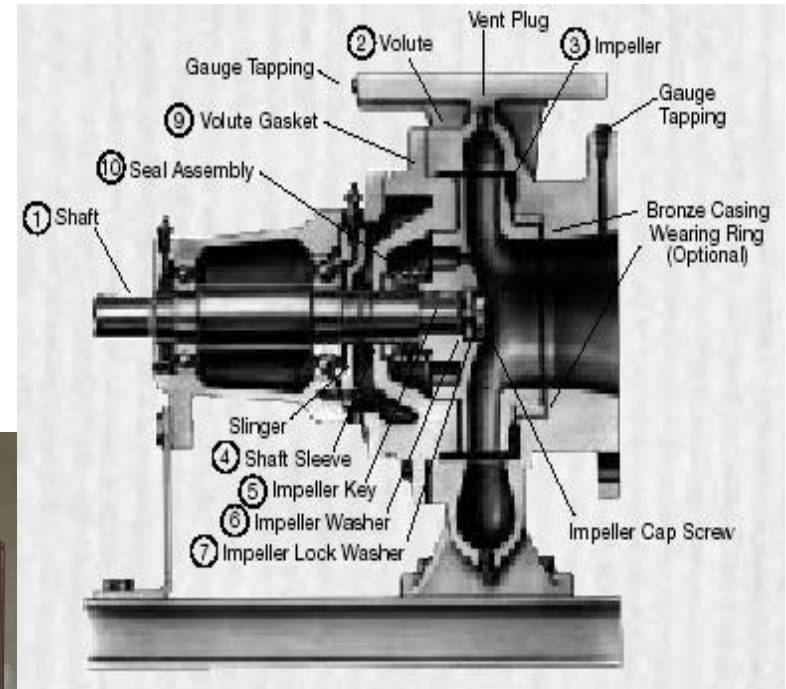
## Results:

- Actual: 775 gpm w/10-3/8" imp
- 3.1% below design
- Steep Pump Curve –  
Immediate Resolution.



# Pump Flow Measurement

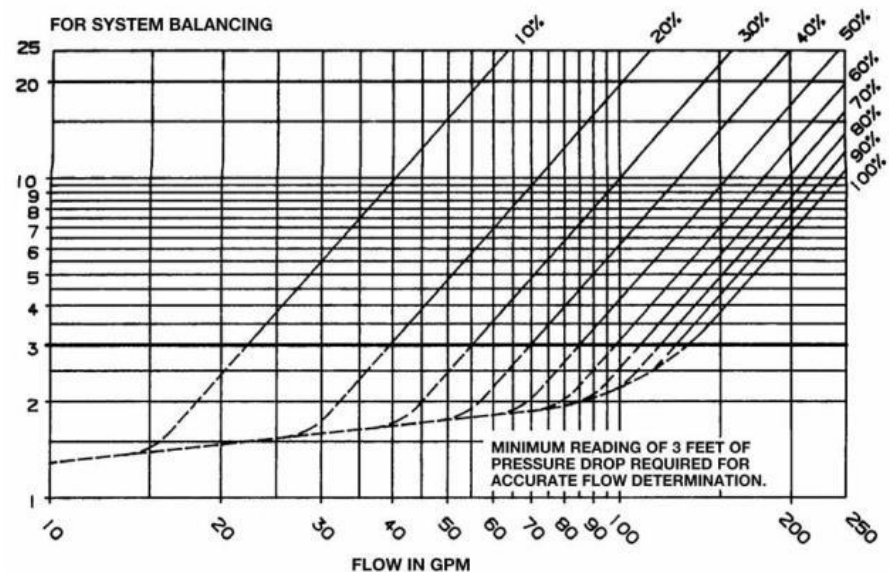
- Provide test ports/pump taps at the pumps (Extend outside of insulation).
- Provide a flow measuring device at the pump  
Fixed orifice type device preferred, use Multi-Purpose Valves with **caution (sized properly)**.





# Water Flow Measuring Stations: Sizing

- ❑ Flow measuring stations need to be sized to allow for a measurable and useful pressure drop.
  - ❑ Size the FS for water **flow quantity** and not **pipe size**
- ❑ The use of Multi-Purpose Valves for total pump flow measurement
  - ❑ Typically sized line size and not for flow quantity (oversized)
  - ❑ Location is not ideal, need 5 pipe diameters before and after the valve.



# Water Flow Measuring Stations: Strainer Effect

**$\frac{3}{4}$ " Balancing Valve  
50% Open**



**$\frac{3}{4}$ " Balancing Valve  
25% Open**

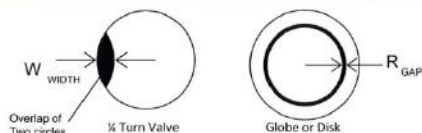




# Water Flow Measuring Stations: Strainer Effect



## Strainer Effect on Low Flow Globe Style Manual Valves



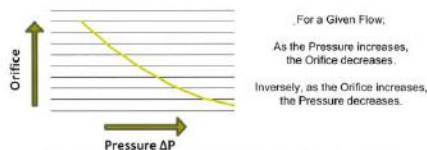
Pressure $\Delta P$	Area In <sup>2</sup>	Max Gap 1/2 Turn Valve	Max Gap Globe Style
2	0.0186	0.074	0.0108
5	0.0118	0.054	0.0085
10	0.0083	0.042	0.0072
20	0.0059	0.034	0.0060
30	0.0048	0.030	0.0054

All smaller than  
10 mesh screen

The calculations on this document are generalized due to the Flow Coefficient (K) being unknown and varying for diverse flow orifice conditions. While changes in K do effect the orifice size, these orifices are still very small for low flows. It is the purpose of this document to demonstrate that these orifices are often smaller than the strainer mesh openings, not to determine the exact size of the orifice for a given flow. The physical configuration of the gap from the Globe Design is smaller than the mesh opening for low flow requirements while a quarter turn valve allows for optimal orifice size for a manual balancing valve.

### 1.0 GPM Flow - Calculated

Estimates of Area which vary depending on Coefficient of Discharge



General Relationship of Orifice/Pressure for a Given Flow

According to ASTM E 11-04  
Specifications

Approximate Opening:  
U.S. No 10 Test Sieve - 0.078"  
U.S. No 20 Test Sieve - 0.033"

Equation to Determine Approximate  
Orifice for a Given Flow

$$A = \frac{Q}{25K\sqrt{\Delta P}}$$

Equation to Determine Max Gap  
using Disk or Globe Restriction

$$R_{GAP} = R - \sqrt{R^2 - \frac{A}{\pi}}$$

Q = Flow  
A = Area  
K = Flow Coefficient = 1  
P = Pressure Differential  
R = Radius of Orifice

NOTE: Actual orifice dimensions  
will vary depending on the flow  
characteristic

Equation to Determine Center of Two  
Circles Given Known Area of Overlap

$$A = r^2 \cos^{-1} \left( \frac{d^2 + r^2 - R^2}{2dr} \right) + r^2 \cos^{-1} \left( \frac{d^2 + R^2 - r^2}{2dR} \right) - \frac{1}{2} \sqrt{(-d+r+R)(d+r-R)(d-r+R)(d+r+R)}$$

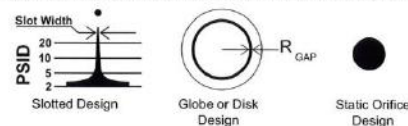
$$r = R = \text{Ball I.D.} = 0.5$$

Equation to Determine  
Width of Overlap  $W_{\text{WIDTH}} = 2R - d$



## Variable Orifice Strainer Effect Under Low Flow Conditions

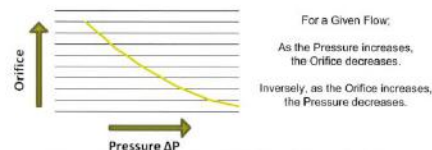
For a given differential, the slotted and globe design have the same area.



Pressure $\Delta P$	Slot Width	Disk Gap (R-GAP)	Diameter of Static Orifice	Area In <sup>2</sup>
2	0.350	0.0108	0.165	0.0186
5	0.060	0.0085	0.165	0.0118
10	0.015	0.0072	0.165	0.0083
20	0.008	0.0060	0.165	0.0059
30	0.002	0.0054	0.165	0.0048

### 1.0 GPM Flow - Calculated

Estimates of Area which vary depending on Coefficient of Discharge



General Relationship of Orifice/Pressure for a Given Flow

The calculations on this document are generalized due to the Flow Coefficient (K) being unknown and varying for diverse flow orifice conditions. While changes in K do effect the orifice size, these orifices are still very small for low flows. It is the purpose of this document to demonstrate that these orifices are often smaller than the strainer mesh openings, not to determine the exact size of the orifice for a given flow. The physical configuration of a Slotted Orifice or the gap from the Globe Design is smaller than the mesh opening for low flow requirements. A Static Orifice Pressure Independent design allows for optimal orifice size for an automatic flow limiting valve.

### WARNING: Cascade Failure Can Occur with a Variable Orifice Design!

Why? These are pressure dependent for position (P1, P2). As the orifice becomes clogged, the differential pressure increases resulting in the piston closing further with even smaller orifices that clog more quickly. Cascade failure is imminent with total stoppage of flow once clogging begins.

Equation to Determine Approximate  
Orifice for a Given Flow

$$A = \frac{Q}{25K\sqrt{\Delta P}}$$

Equation to Determine Max Gap  
using Disk or Globe Restriction

$$R_{GAP} = R - \sqrt{R^2 - \frac{A}{\pi}}$$

Q = Flow  
A = Area  
K = Flow Coefficient = 1  
P = Pressure Differential  
R = Radius of Orifice

NOTE: Actual orifice dimensions will  
vary depending on the flow coefficient

Equation to Determine Gap / Width  
of Slotted Design

Taken from Actual Measurements

# Water Flow Measurement: Automatic Flow Limiting Devices

- These devices do not eliminate water balancing.
- Ideal for fan coil units, unit ventilators, heat pumps, VAV reheat coils and areas where access to valves is limited (**actual pressure readings might not be obtained for each auto-flow**).
- Factory-installed piping kits frequently do not provide access to the ports!!!
- Make sure they get installed in the correct locations, **per GPM not just pipe size**.

# Water Flow Measurement: Factory-Piped Balancing Valves

